

Oxyfuel Research at RWE npower plc.

The CRF 2012 Annual Meeting and
Combustion Divisional Seminar,
25th April 2012.

Gerry Riley and John Smart

Presented by Mark Flower



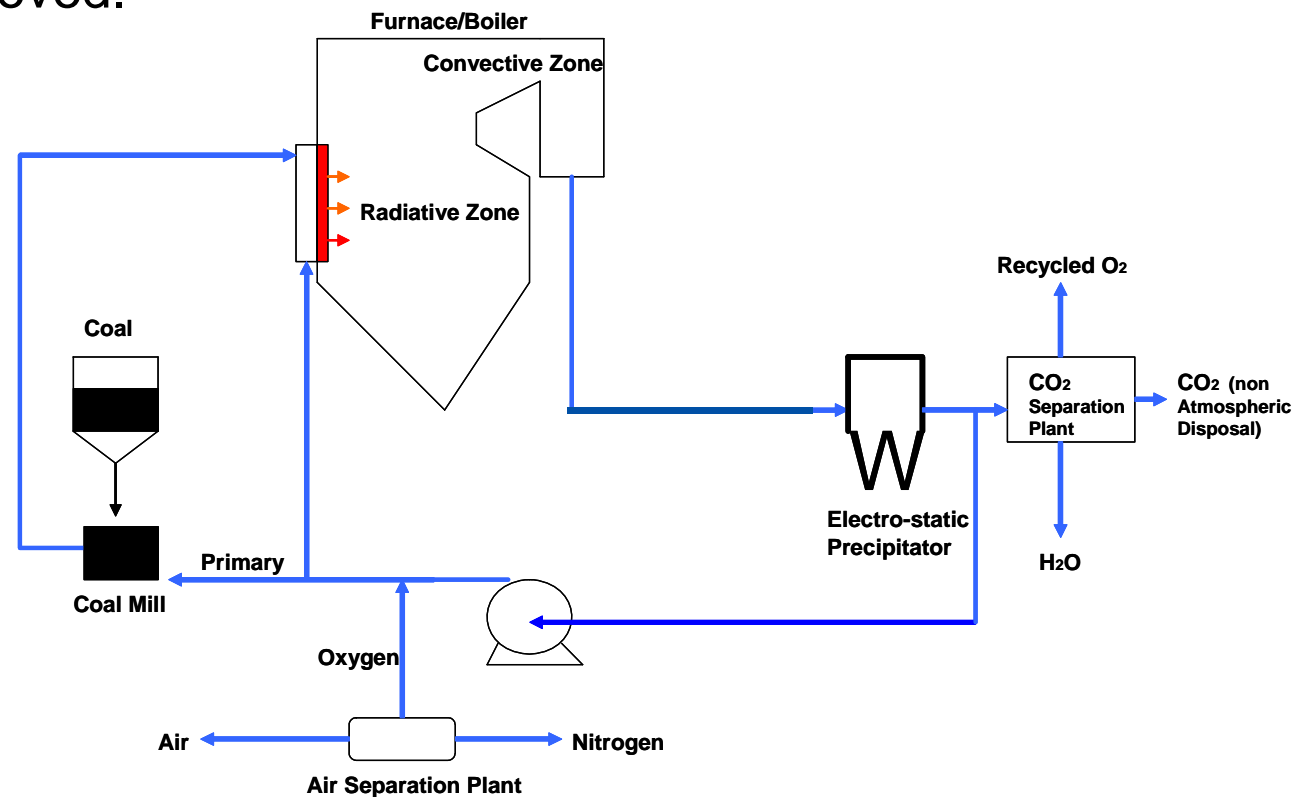
Presentation overview

- Background
- Highlights from Test Programmes
 - Oxyfuel UK DTI Project
 - BOM-COM RFCS
 - EcoScrub RFCS project
 - Fuel project (RWE npower project)
 - Oxygen injection project with BOC
- Summary

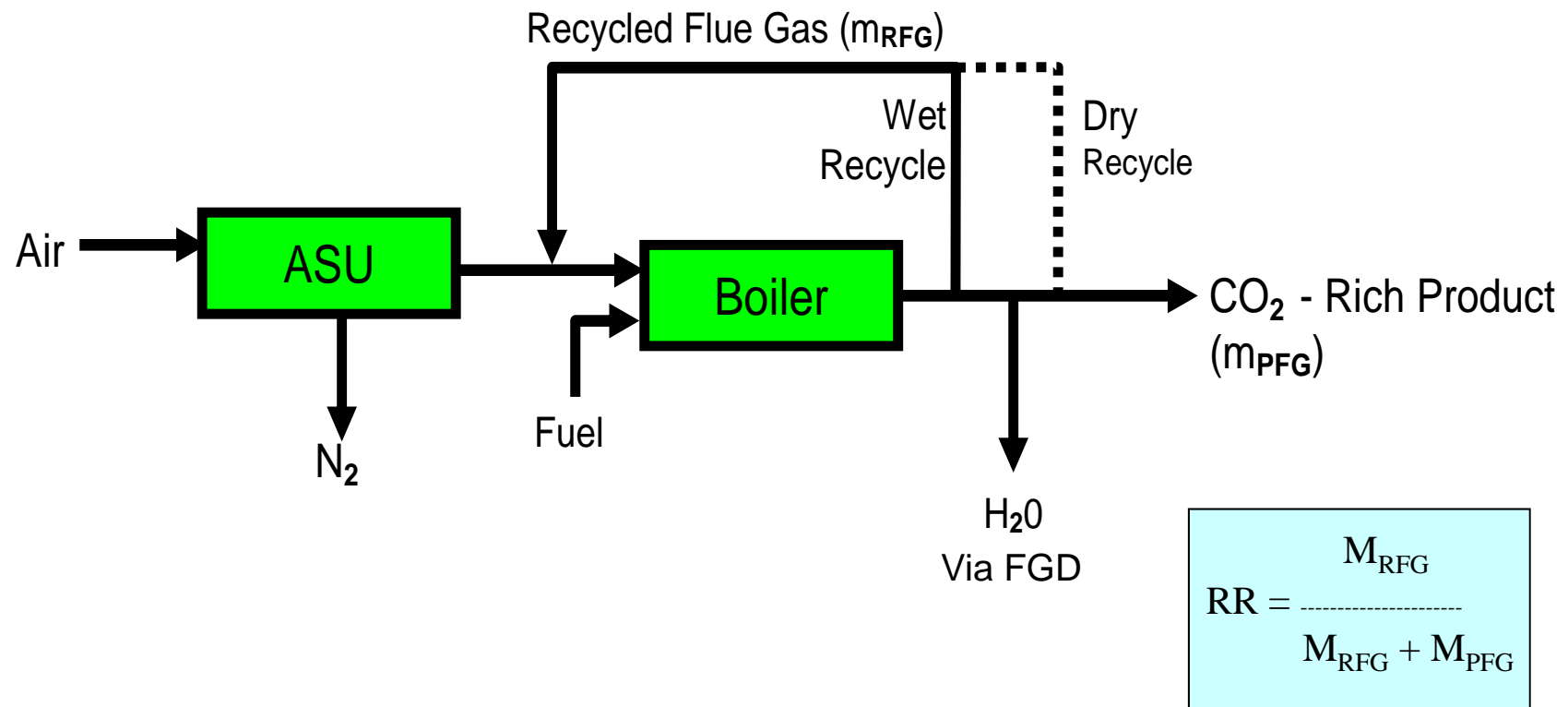


Background: What is oxyfuel?

- > Flue gas is recycled and air is replaced by oxygen
- > The gas inside the boiler becomes almost nitrogen-free and CO₂ is then removed.



Background – Recycle Ratio



Overview of CTF programme

CTF Studies

Safety

Fuel Issues

Optimisation

**Process
Development**

**Desktop
Studies**

Overview of CTF programme

- Safety handling and storage of oxygen and CO₂
- Flame detection issues (higher moisture and CO₂ may affect UV and IR absorption)
- Safety of mixing oxygen/CO₂
- Flame stability
- Safe switch-over the oxyfuel combustion
- Safety of staff with CO₂ /flue gas leaks etc.
- Purging for safety

- Air leakage
- Optimum recycle ratio
- Air heater design
- Optimisation of mixing strategy (where to add O₂ - PA/SA/TA etc.)
- Gas recirculation
- Oil burner operation on oxyfuel
- Flexibility - start-up/shutdown limited by air separation unit so cold-start on air

- Selection of coals (optimise purchasing)
- Use of biomass
- Furnace slagging
- Furnace Corrosion
- Fouling
- NO_x (chemistry not well understood)
- Heavy metal recycling and ash composition

- Burner design
- Carbon burnout
- Heat transfer (radiative/convective properties)

- Regulation issue - LCPD limits for oxyfuel
- Pre-investment issues (upfront parameters)
- Required footprint for retrofit (e.g. air separation unit)

CTF oxyfuel conversion

- > Two-stage conversion of the CTF
 - Phase 1: Stored CO₂ injection
 - Phase 2: Flue gas recirculation
- > Why a two-phase strategy?
 - Rapid start-up with less (though significant) engineering – air ingress
 - Flexibility
 - Identify show stoppers or new issues at an early stage
 - Second stage to quantify full impact of issues such as NO_x, slagging, corrosion and trace elements that cannot be fully studied by CO₂ injection alone

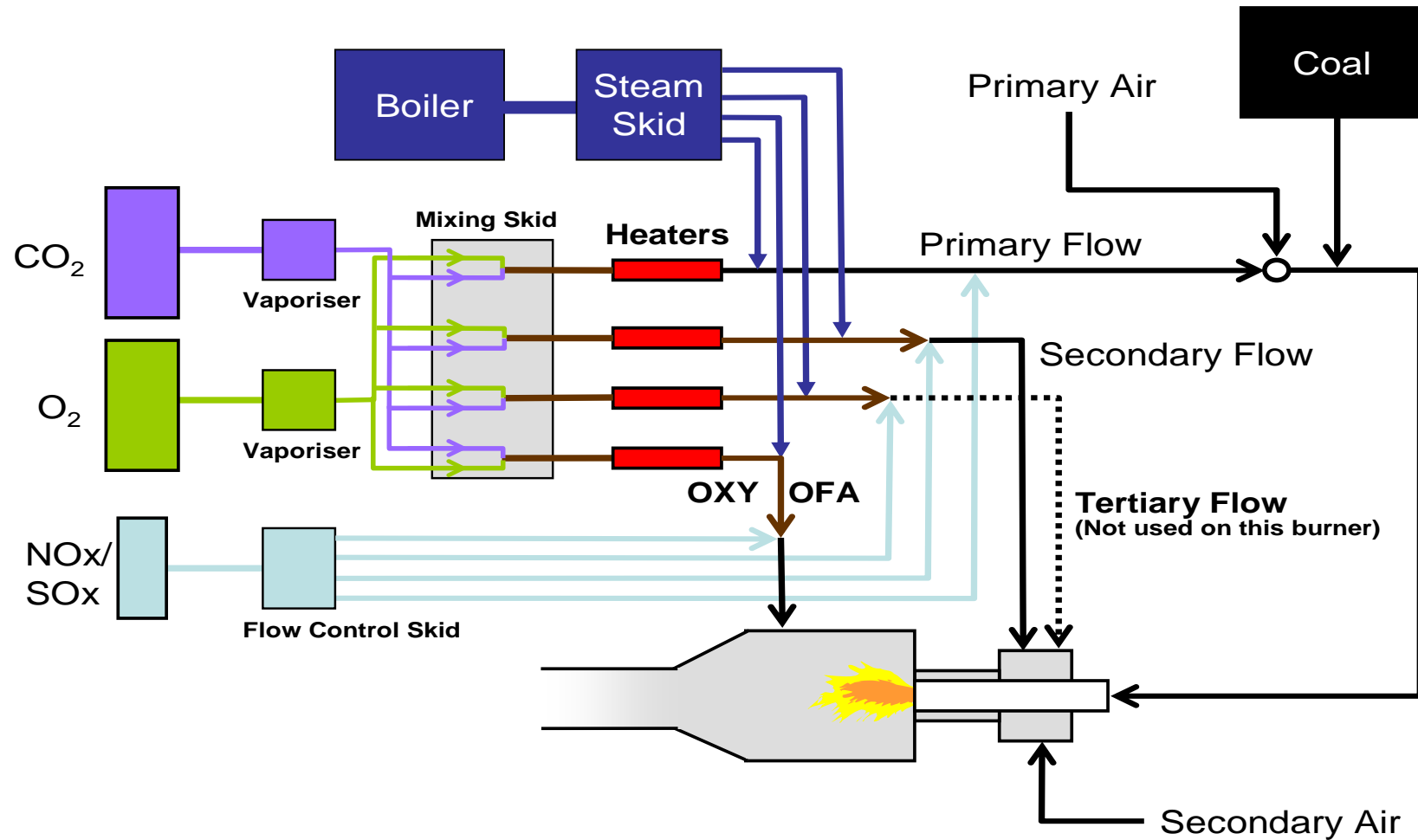
CTF oxyfuel conversion

- > Two-stage conversion of the CTF
 - Phase 1: Stored CO₂ injection
 - **– Cancelled following strategic review**
- > Why a two-phase strategy?
 - Rapid start-up with less (though significant) engineering – air ingress
 - Flexibility
 - Identify show stoppers or new issues at an early stage
 - **– Cancelled following strategic review**

Rig modifications

- > CO₂ injection
 - Storage tanks for O₂ and CO₂ with mixing and safety systems
 - Modified system of blowers and SA/TA heaters
 - Steam boiler
 - Doping gasses (SO_x, NO_x)
 - Controls and logic interface with existing CTF system

Schematic of Once Through Oxy-Fuel System



RWEnpower's OxyFuel facility



**O₂, CO₂ and N₂
Storage Vessels**

RWEnpower's OxyFuel facility



Evaporators

RWEnpower's OxyFuel facility



Gas mixers

RWEnpower's OxyFuel facility



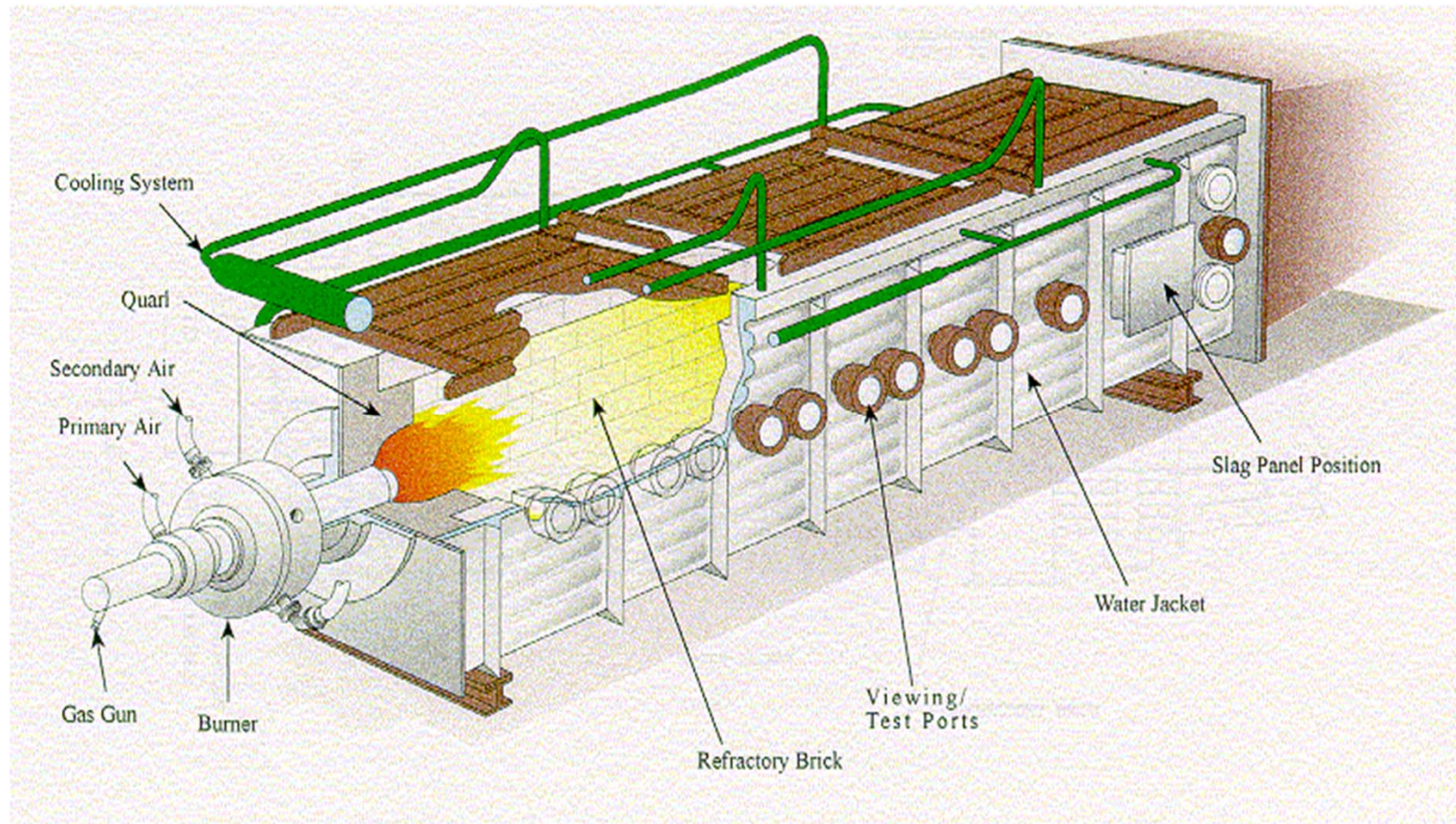
Gas Heaters

RWEnpower's OxyFuel facility



Burner

Schematic of CTF Test Furnace

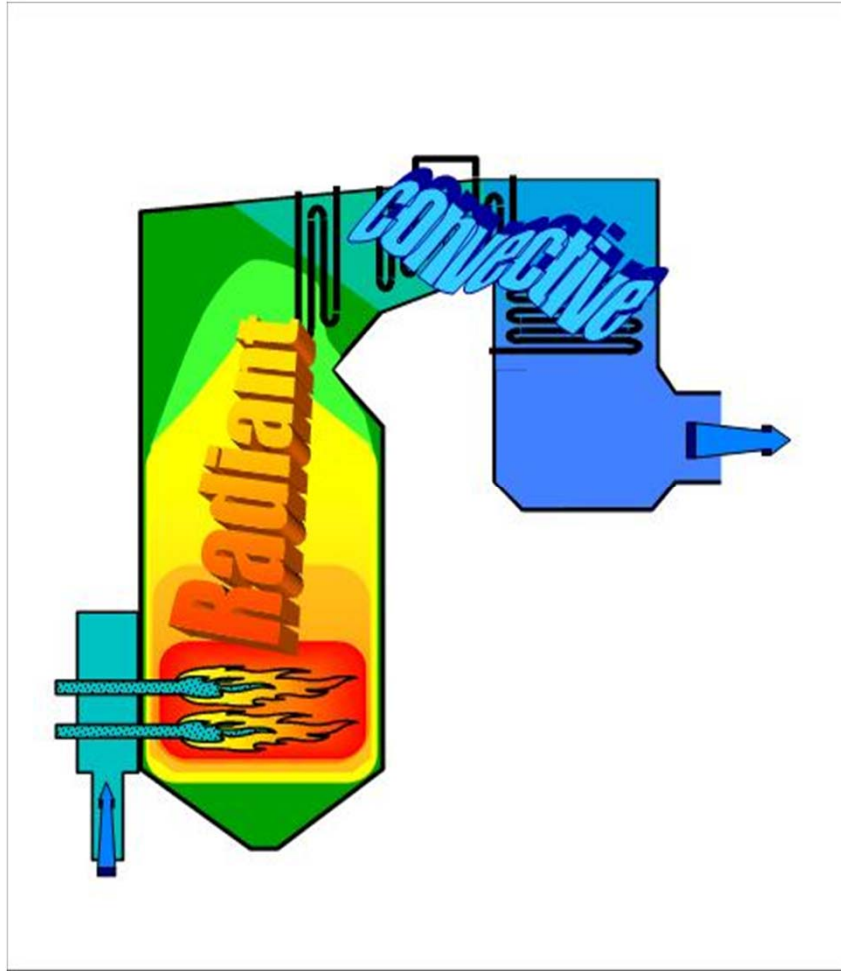


BOFCOM

Heat Transfer under OxyFuel Firing Conditions

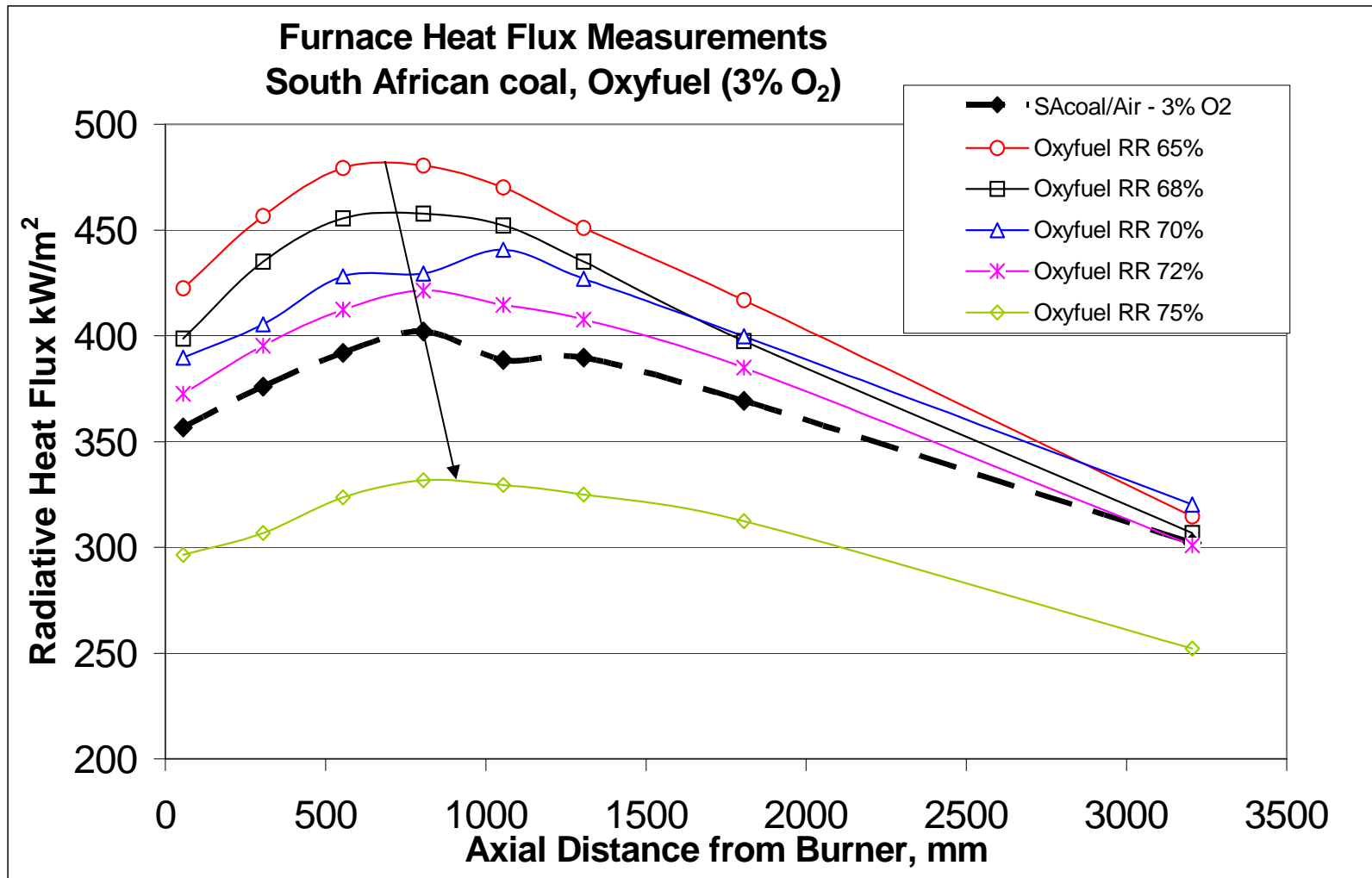


Driver for Studying Heat Transfer Distributions – Radiative and Convective

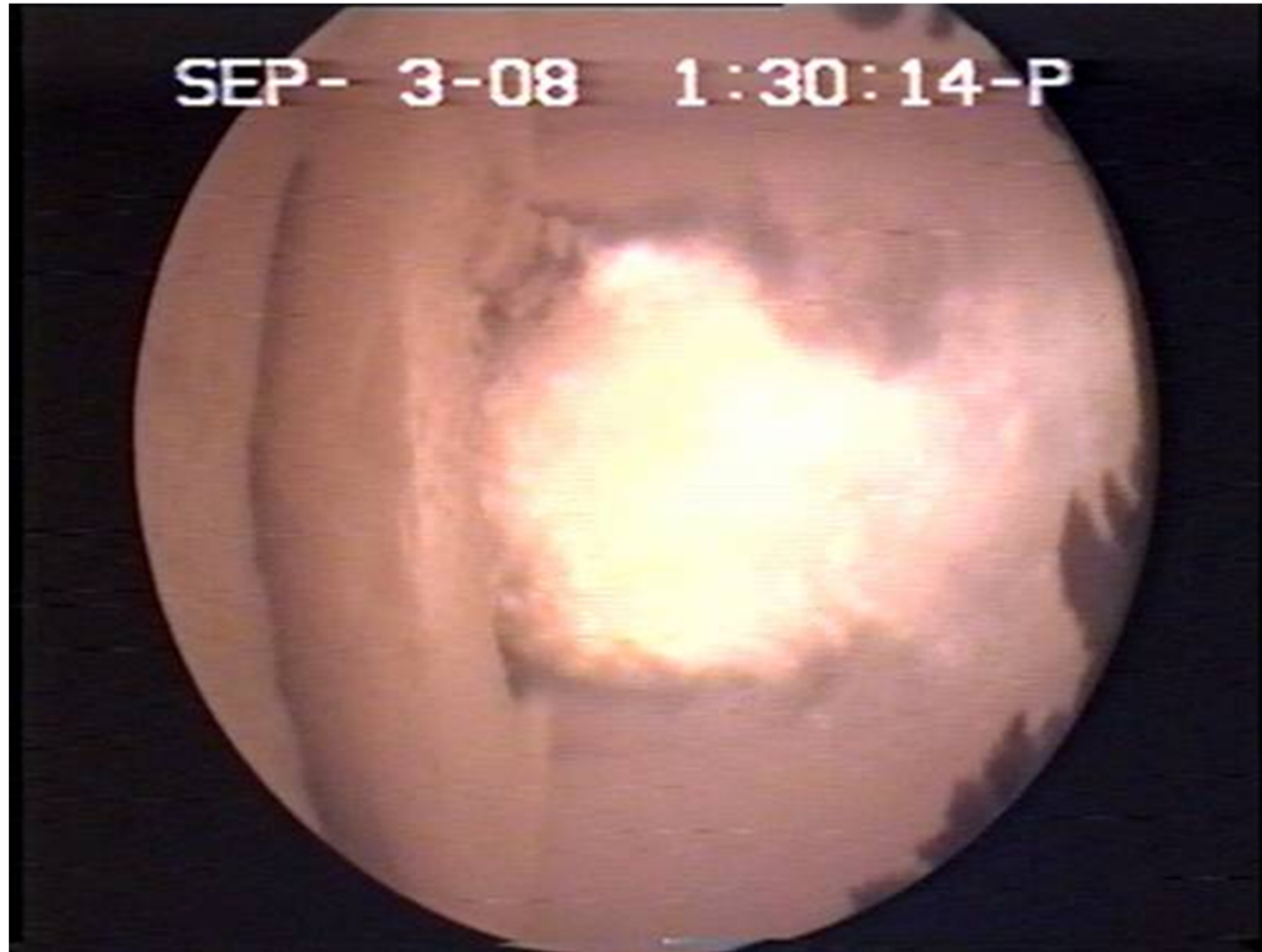


- Radiation heat transfer is driven by gas temperature (T^4) while convective heat transfer by gas temperature and velocity.
- To operate as “air equivalent” the balance between radiative and convective heat transfer has to be found
- The recycled flue gas can be either wet or dry dependent on where the recycled flue gas taken from in the system.
- The recycled flue gas could be take wet from the outlet of the ESP (where the moisture content would be circa 18% by volume) or after an FGD system (where the moisture content would be circa 8% by volume).

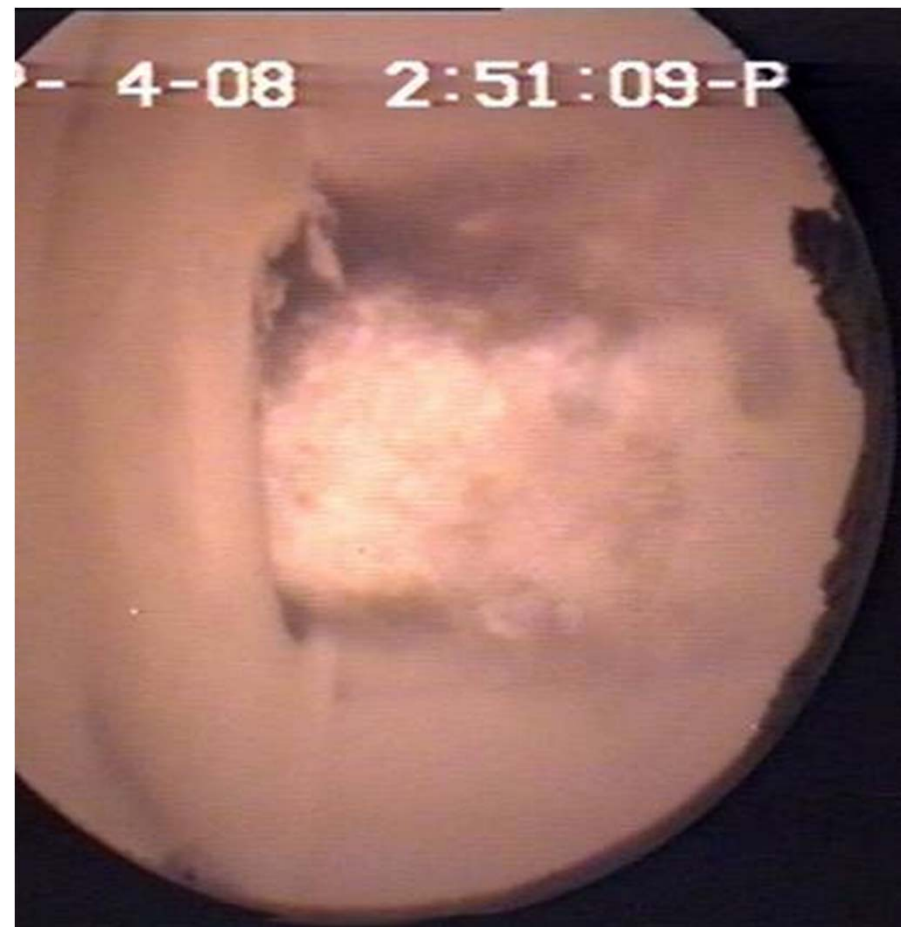
Radiative HT - South African coal – Dry Recycle



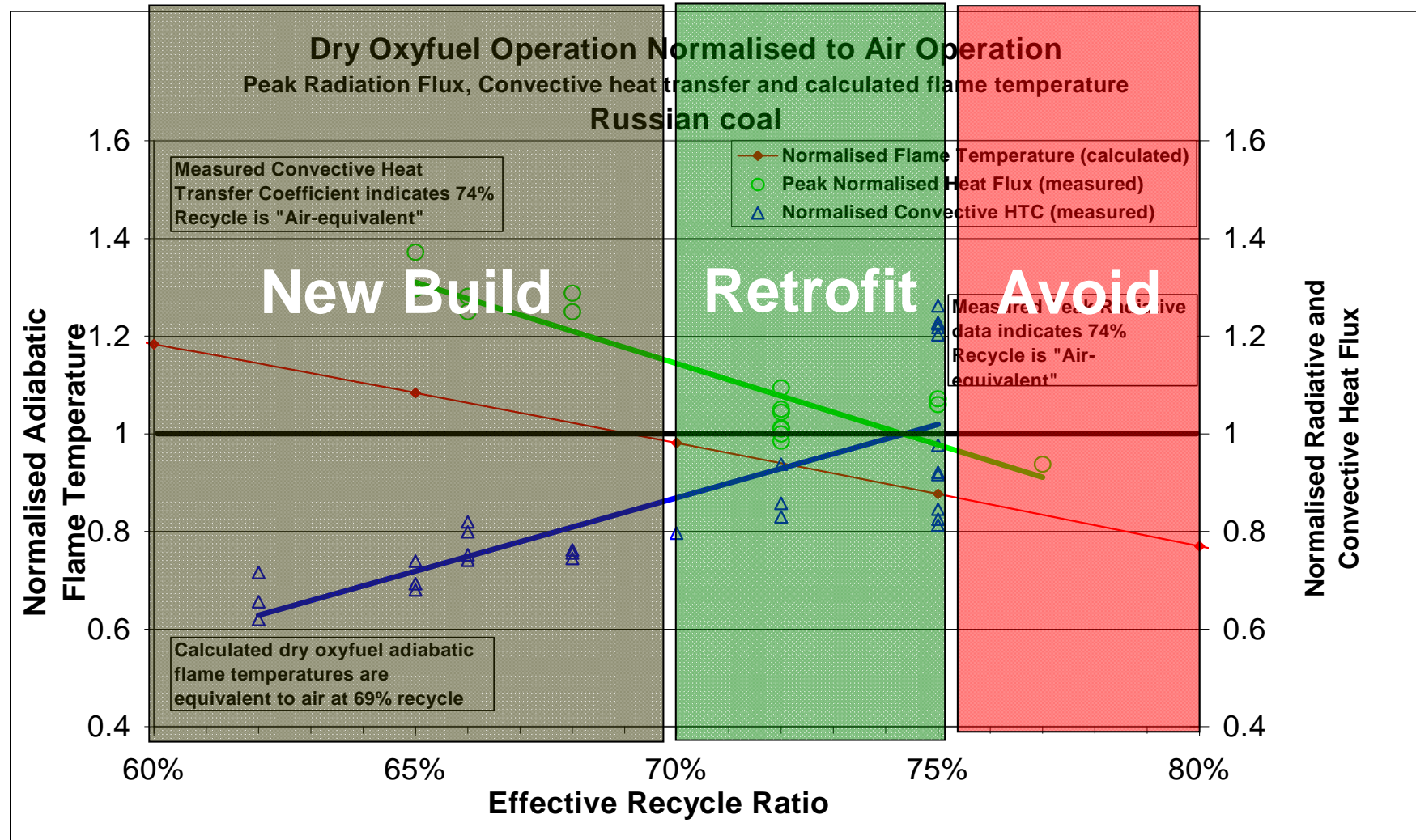
IFRF Burner - RR 66%, 38% Inlet O₂
Hot intense flame



IFRF Burner – RR 77%; 28% Inlet O₂ Cool Flame



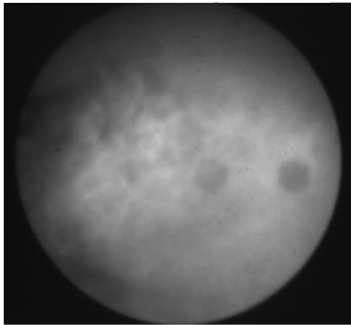
Normalised Convective & Radiative Heat Flux Russian Coal - Dry Recycle



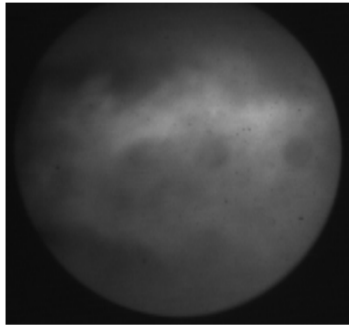
Oxycoal - Flame Stability

Flame Animations (South African Coal)

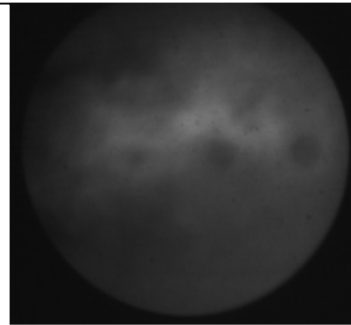
- Images for different simulated recycle rates under low O₂ settings



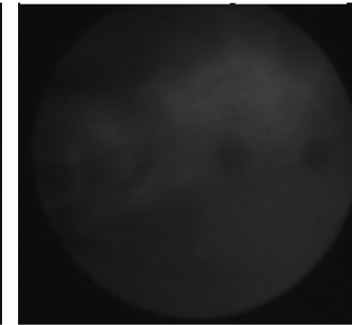
65% rr, Total flow 554.74kg/h
Sec 400kg/h@35.8% O₂
(time: 14:19)



68% rr, Total flow 615.71kg/h
Sec 457kg/h@31.6%
(time: 13:44)

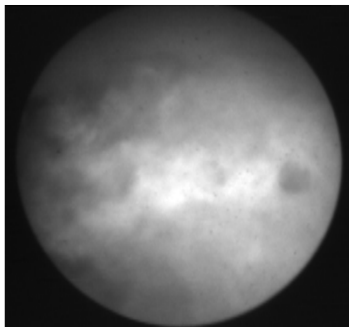


70% rr, Total flow 656.99kg/h
Sec 501kg/h@29.0% O₂
(time: 13:14)

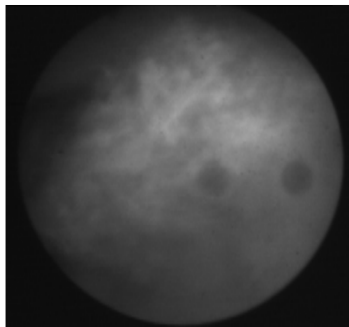


72% rr, Total flow 709.04kg/h
Sec 552kg/h@26.5%O₂
(time: 12:41)

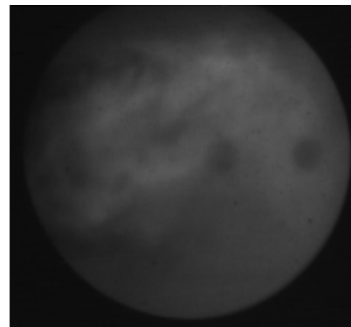
- Images for different simulated recycle rates under high O₂ settings



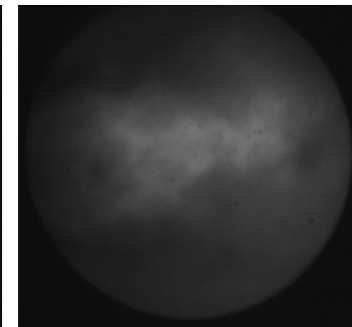
65% rr, Total flow 567.69kg/h
Sec 412kg/h@38.0% O₂
(time: 14:36)



68% rr, Total flow 624.70kg/h
Sec 470kg/h@33.9%O₂
(time: 14:04)



70% rr, Total flow 670.91kg/h
Sec 516kg/h@31.3%O₂
(time: 13:27)



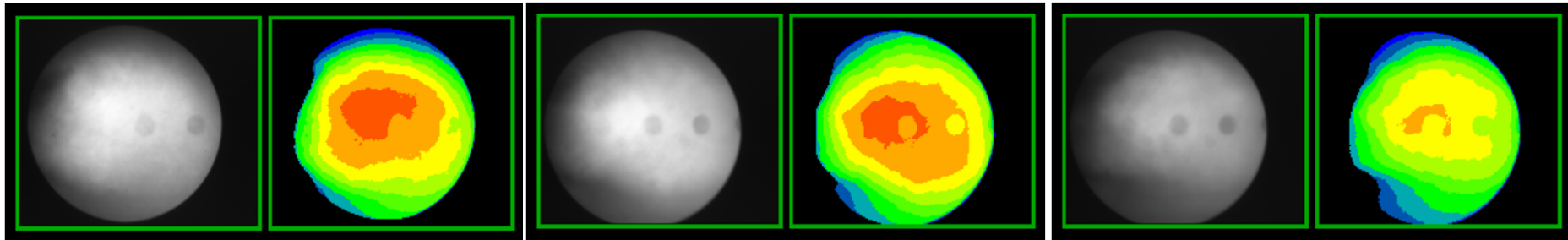
72% rr, Total flow 722.64kg/h
Sec 567kg/h@28.9%O₂
(time: 12:54)



75% rr, Total flow 806.57kg/h
Sec 650kg/h@25.4% O₂
(time: 12:29)

Flame Images

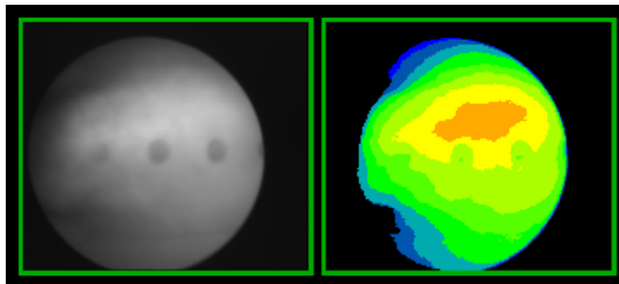
- Temperature profiles for different simulated recycle rates under lower O₂ settings



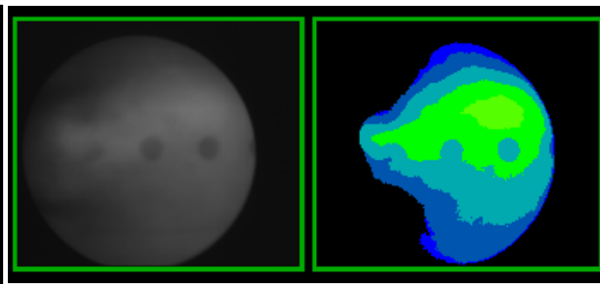
62% RR: Sec.f 322kg/h@39.4%
(time: 12:32, 30-10)

65% RR: Sec.f 368kg/h@34.8%
(time: 15:18, 29-10)

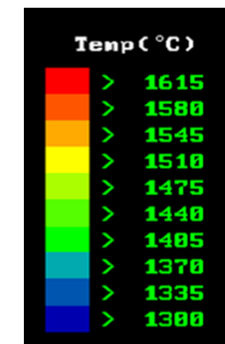
68%RR: Sec.f
422kg/h@30.5%
(time: 15:05, 29-10)



72% RR: Sec.f 513kg/h@25.5%
(time: 14:18, 29-10)



75% RR: Sec.f 600kg/h@22.1%
(time: 13:41, 29-10)



Note: Images and temperature profiles shown here are averaged for 10 instantaneous readings over about 2 minutes.

Conclusions (Dry recycle data)

- > Air operation radiative heat flux found to be equivalent to 72 – 75% recycle ratio (due to different radiative properties of carbon dioxide compared to nitrogen)
- > Radiative heat flux peak shifts downstream as recycle rate increases
- > Convective Heat Transfer equivalent to air at 74% recycle ratio (main factors here are temperature and mass flow)
- > Working range exists (there is a recycle ratio for which both radiative and convective transfer can be reasonable matched between air and oxyfuel operation. It is therefore possible to design a boiler for efficient operation in both oxyfuel and air conditions).
- > Flame stability decreases with increasing recycle ratio

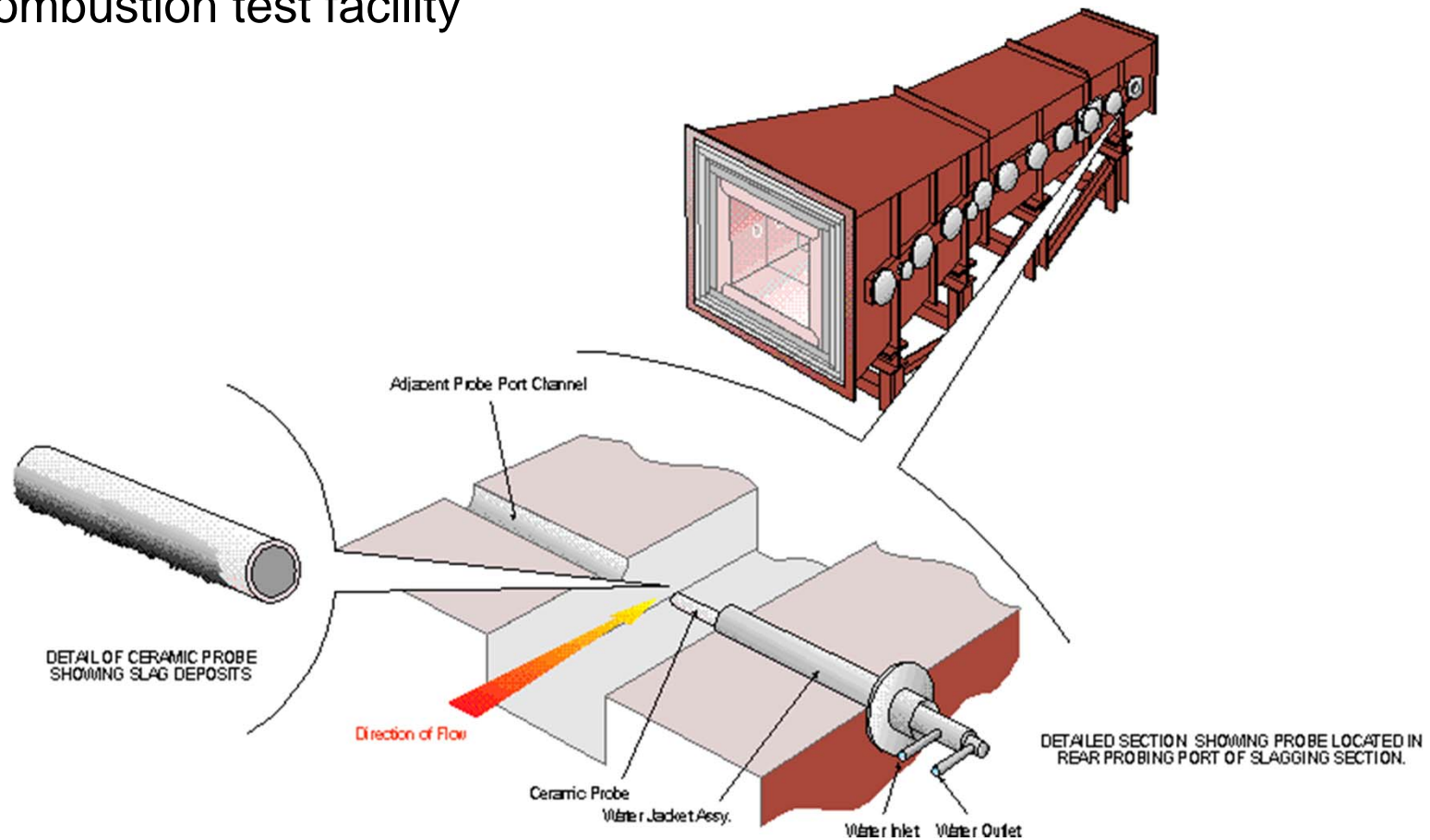
BOFCOM

Deposition Studies under OxyFuel Firing Conditions

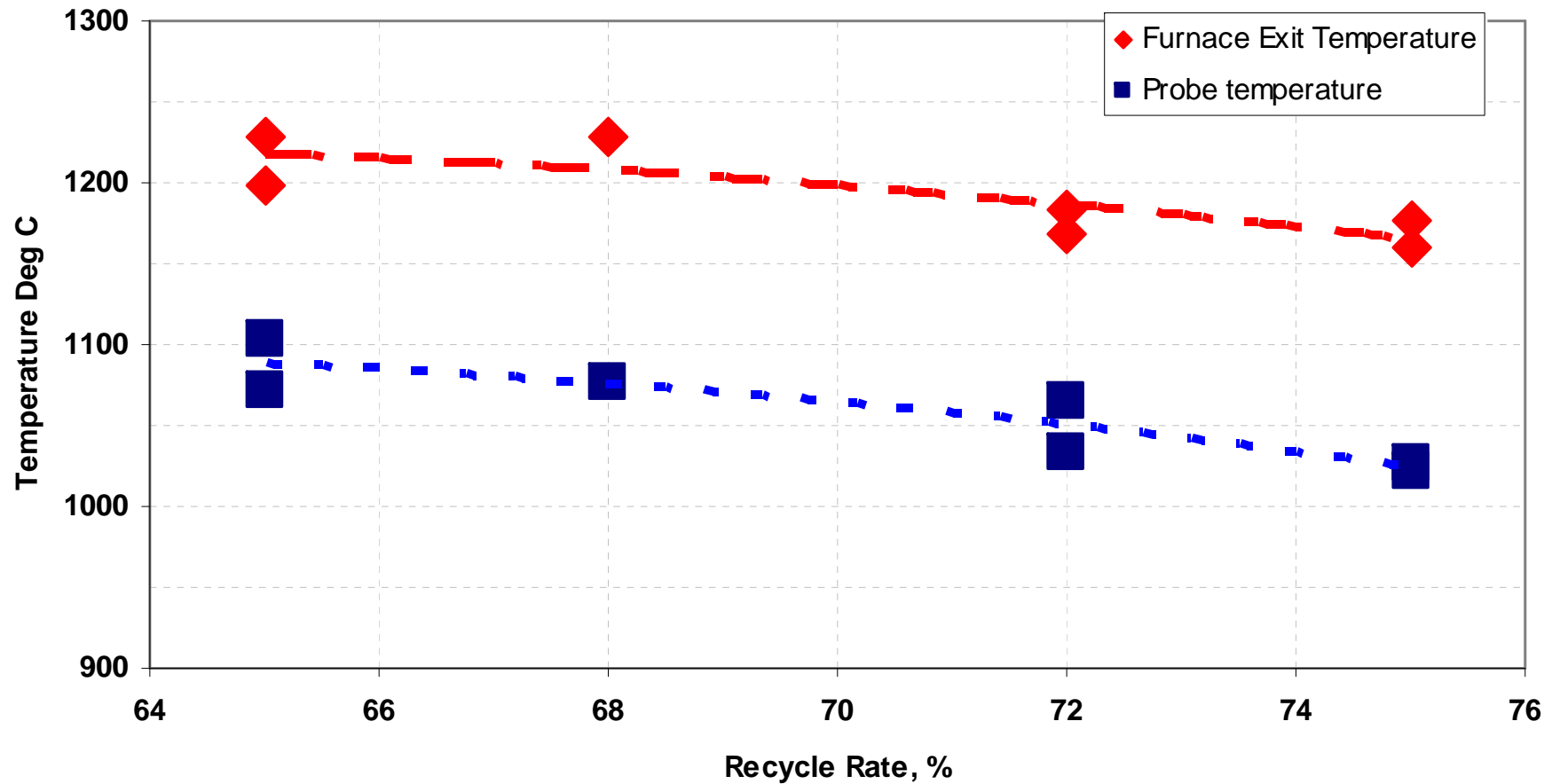


Combustion Test Facility

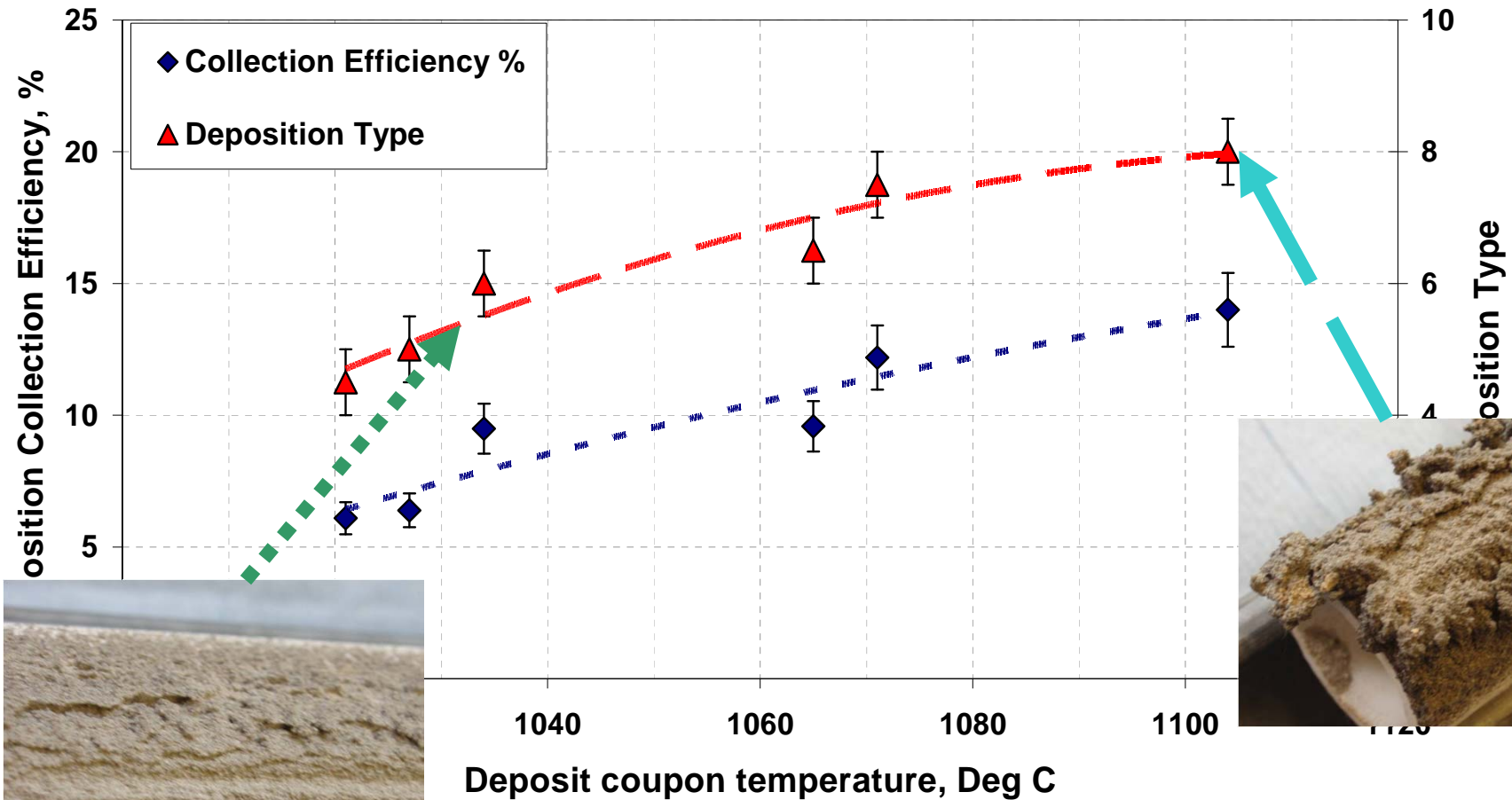
RWE have carried out a series of deposition runs on their pilot scale combustion test facility



Bofcom Deposition Data – Russian Coal 2

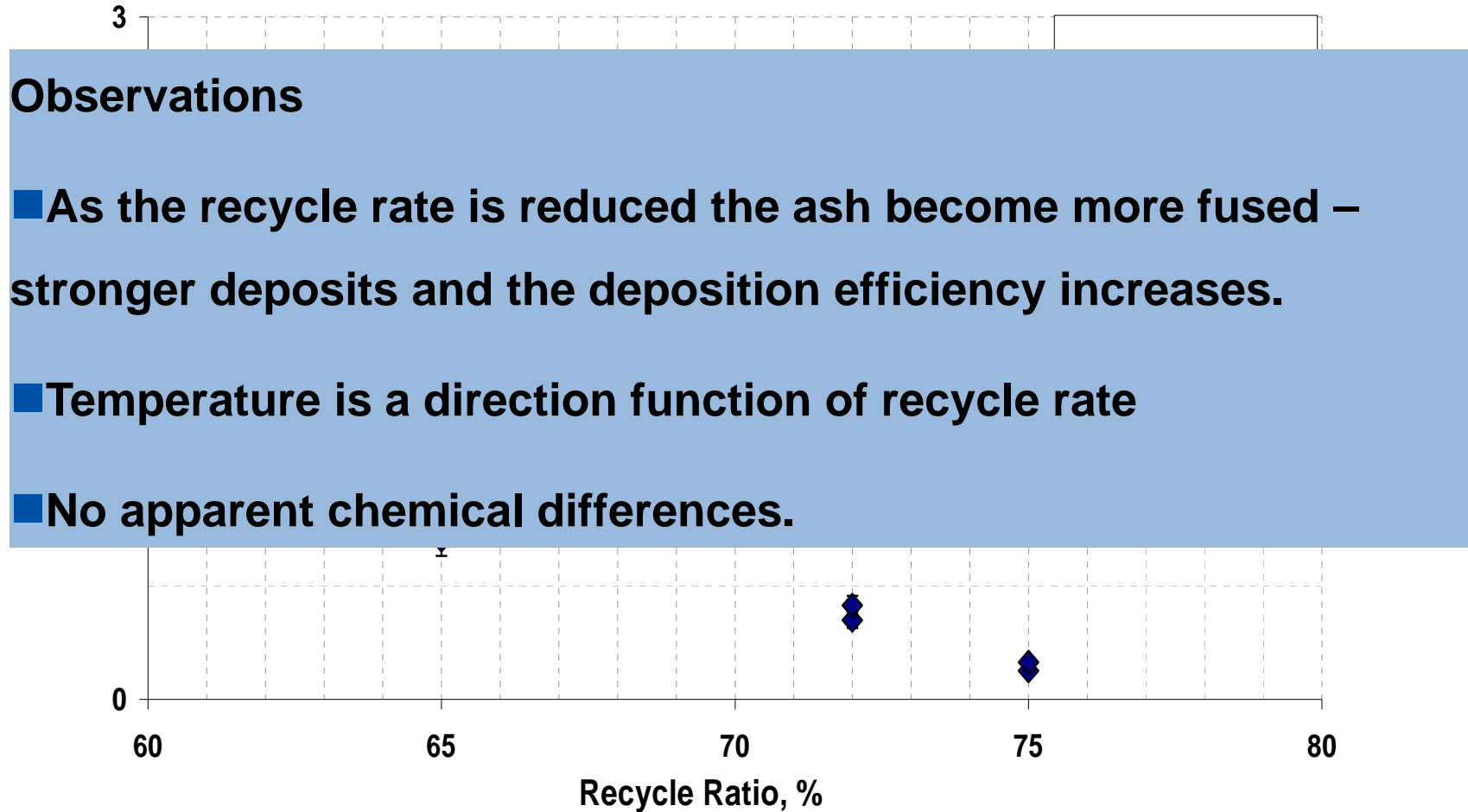


Deposition efficiency and Deposit Type

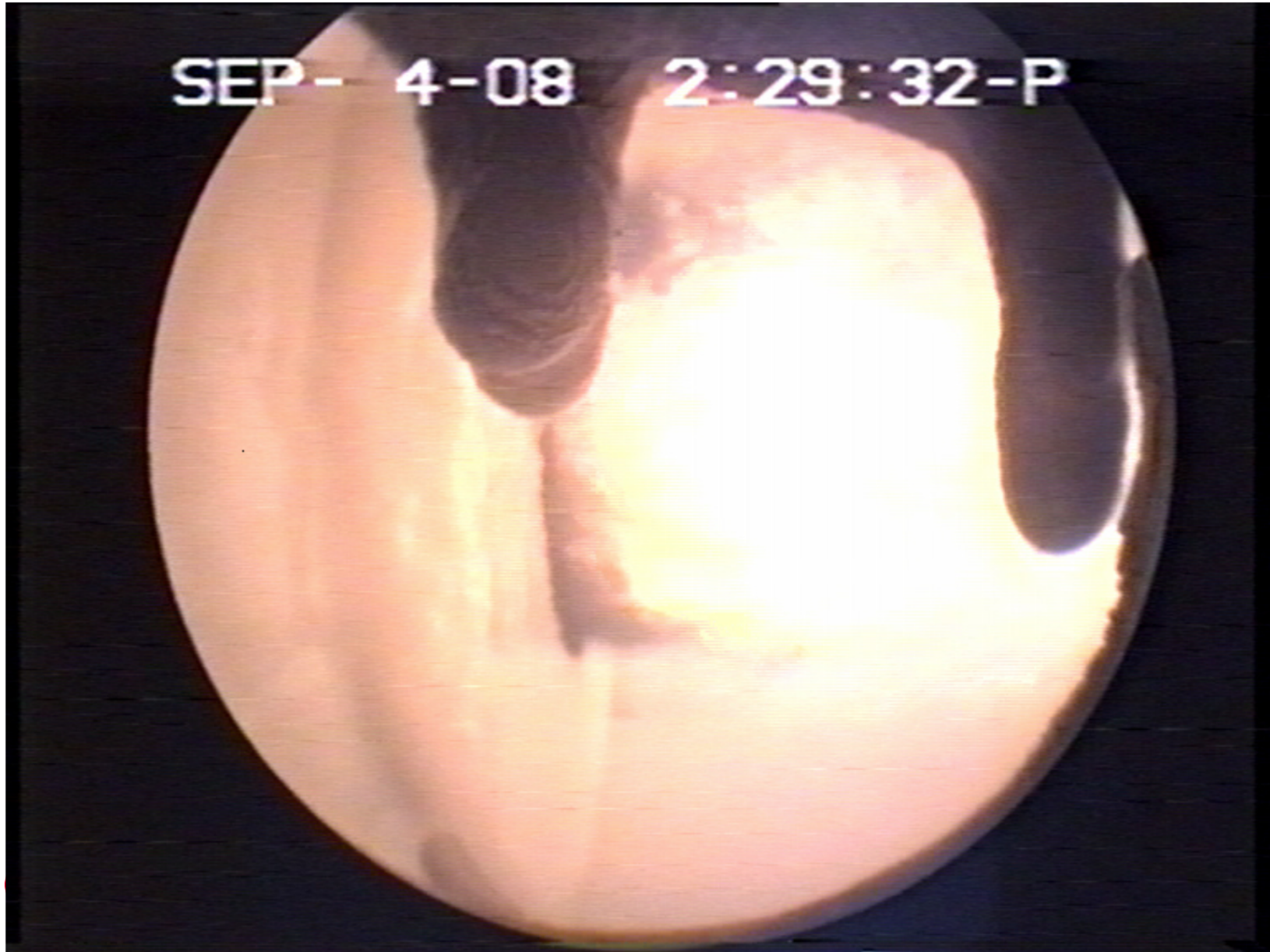


- Amount of ash sticking to probe / ash impacting on probe}

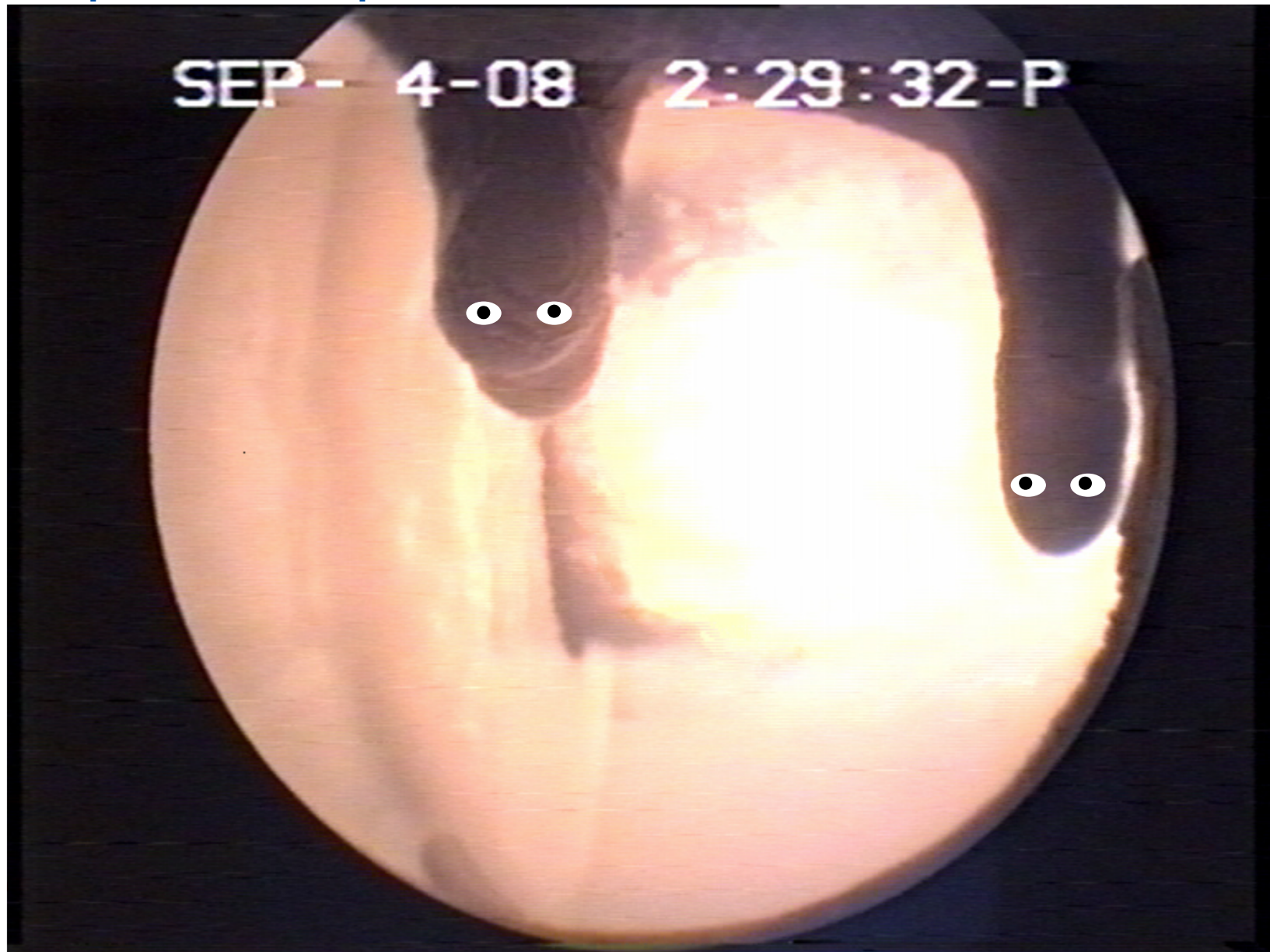
Impact = ***f*** (deposition rate and Deposit type)



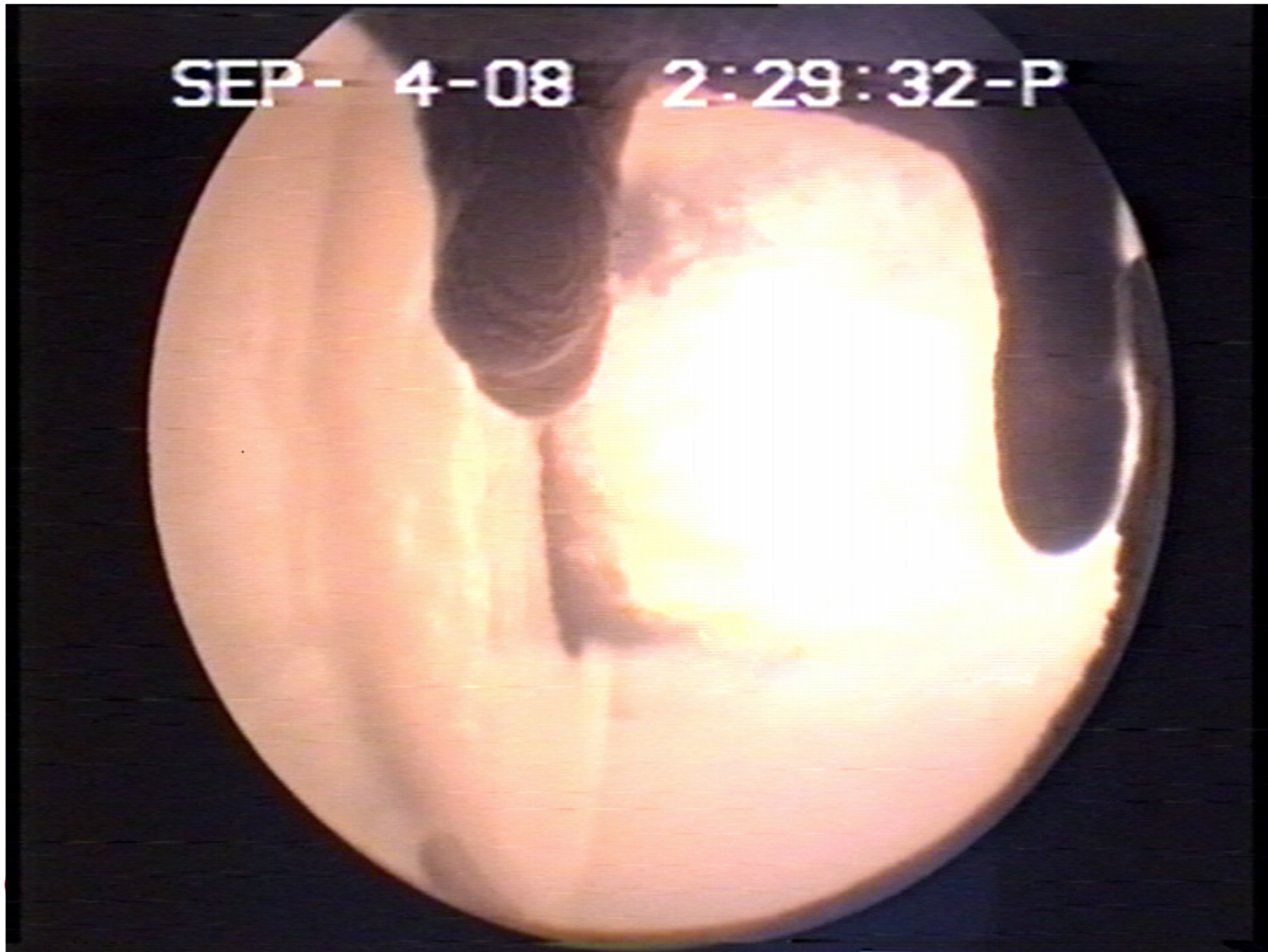
Caption competition!



Caption competition!



Caption competition!



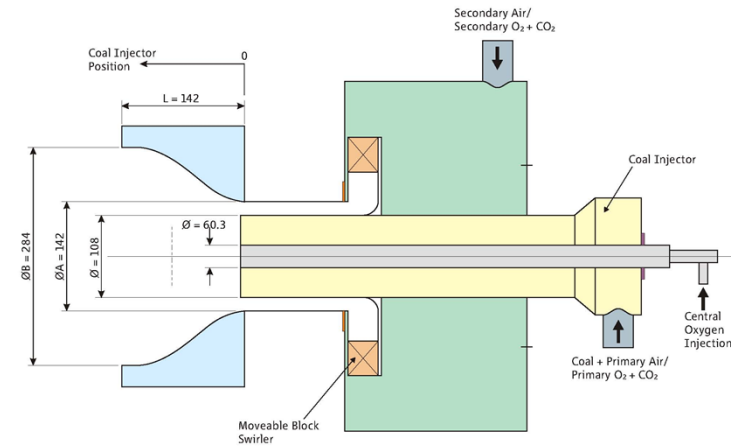
BOC / RWE

Oxygen injection



Oxyfuel with Centre Lance Oxygen injection

- > Injection of pure oxygen centrally through the burner's core air tube instead of through the secondary air register.
- > Strong impact on the flame
- > Potential reduction in NO_x



RWE

Fuel Flexibility

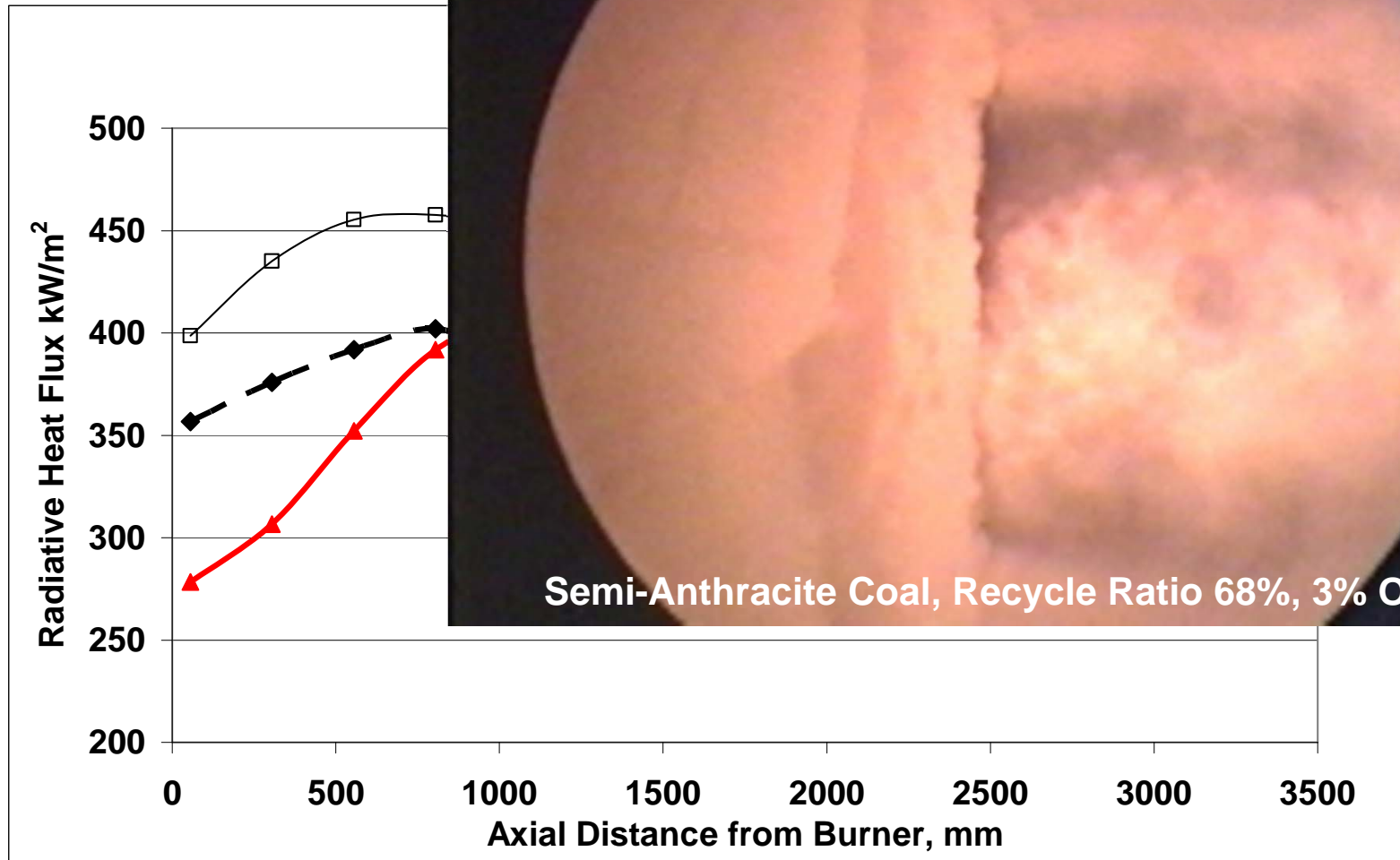


An **RWE** company

RWE npower

PAGE 36

Fuel flexibility



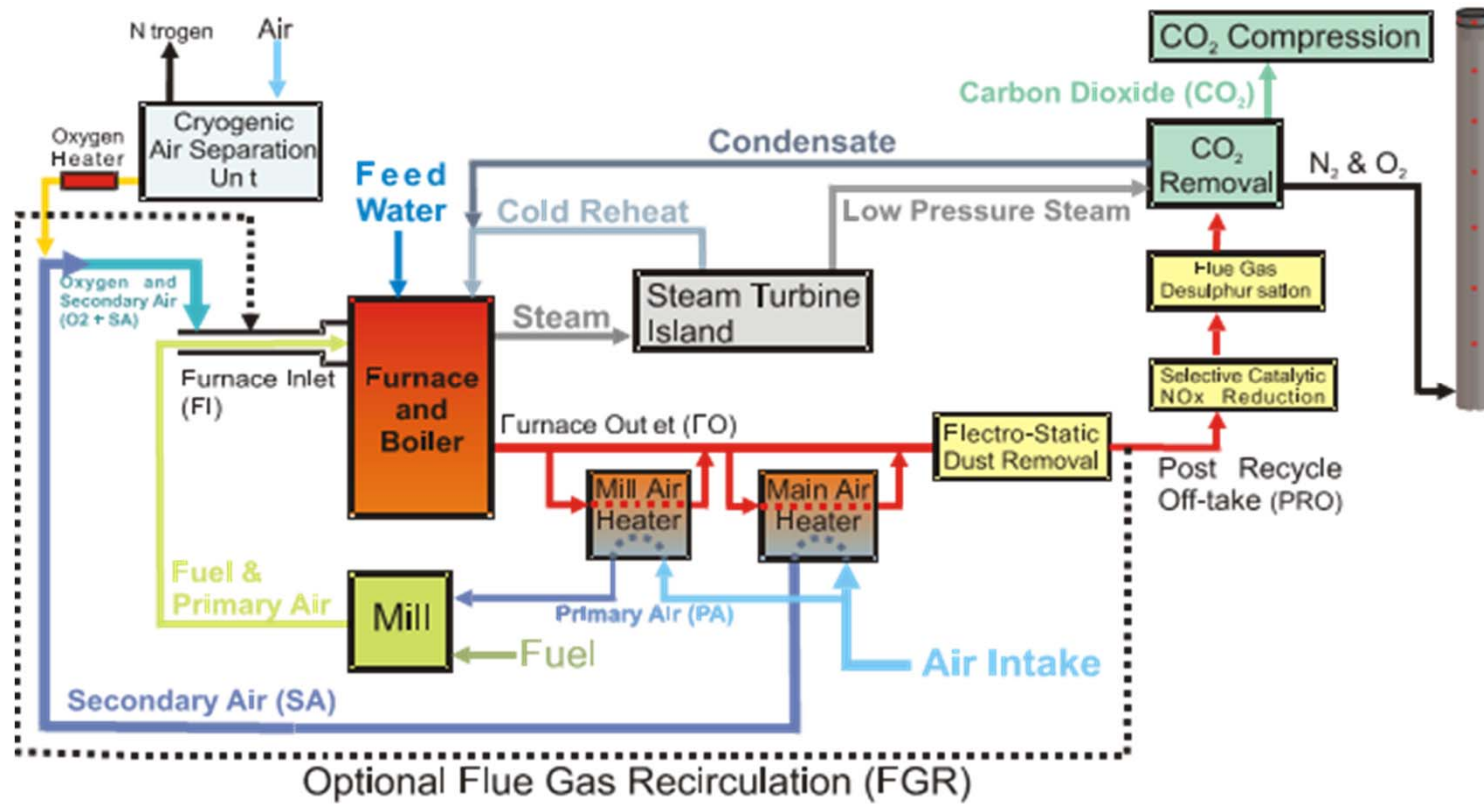
Fuel Flexibility

- > What has been demonstrated is that:
 - Using oxy-fuel combustion technology, a wider range of coals can be fired in a swirl burner configuration for application in wall fired boilers than is conventional with standard air firing.
 - This offers potential for greater fuel type flexibility, wider options in fuel diet and consequential fuels costs than would be normal in a conventional only air fired wall fired boiler.
- > This scoping study has demonstrated that flame ignition, stability and luminosity for low volatile fuel can be improved under oxy-fuel firing conditions compared to air and deserves a more systematic study.

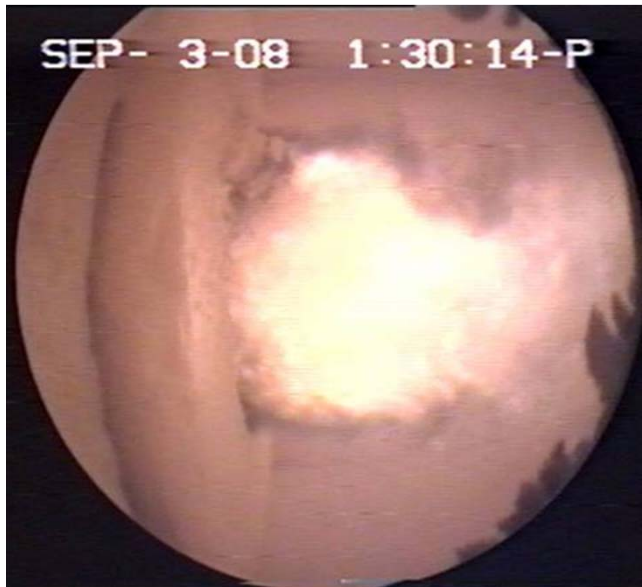
EcoScrub OxyFuel / Post Combustion Capture Hybrid



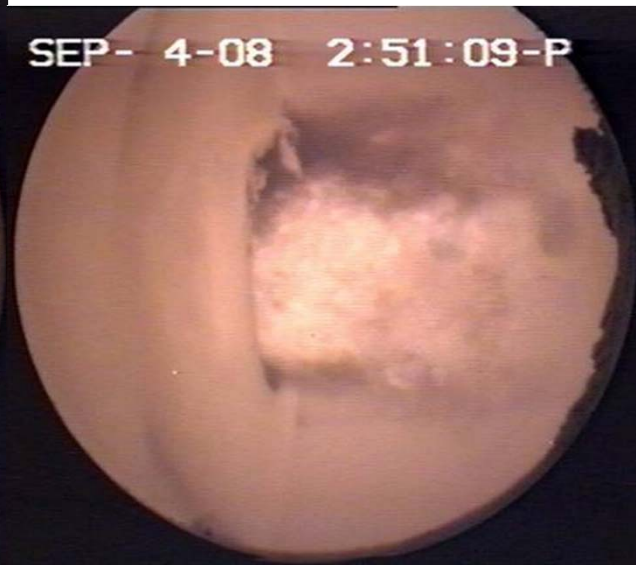
Ecoscrub



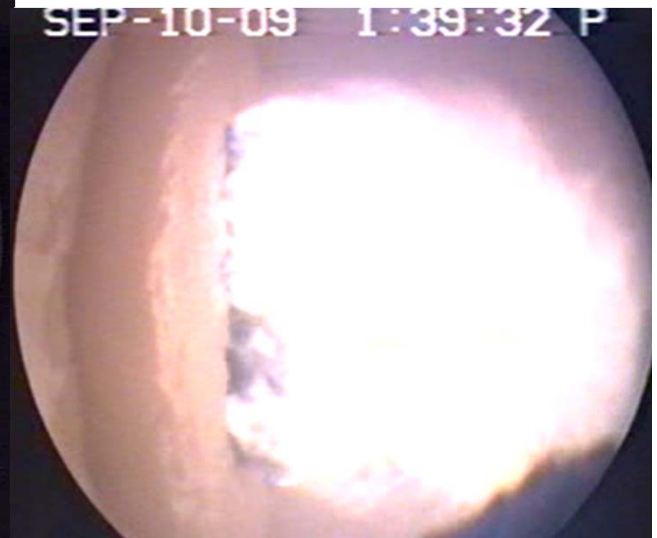
Flames



IFRF Burner - RR 66%, 38% Inlet O₂



IFRF Burner – RR 77%; 28% Inlet O₂



IFRF Burner – ECO Scrub Case 3B
Air as Primary gas!
Reduced heat capacity of N₂ vs CO₂

Some Thoughts

- Development of a low cost option for carbon capture on existing modern coal-fired power plant using a novel combination of techniques employed for CO₂ capture, such as O₂ enrichment and post-combustion solvent scrubbing, together with measures to increase efficiency, reduce steam consumption and generate power requirements.
- Definitely an interesting idea and not crazy but lots of questions to answer
- Demonstrate the ideas
- Commercial – Fuel flexibility; Key pluses over pure OxyF/Amine
- Air ingress

Further work

- Further cost analysis but needs to be site specific
- Future developments in Amines targeted at 28% CO₂ concentration
- Lower cost oxygen production
- Membrane development.



Acknowledgements

- > The combustion test facility conversion to OxyFuel was financed by RWE npower
- > The experimental programmes are co-funded by RWE npower and:
- > The European Commission Research Fund for Coal and Steel - BOFCom
 - Heat Transfer, Wet and Dry recycle, Biomass, OFA, Deposition studies
- > The UK Technology Strategy Board - Oxycoal-UK

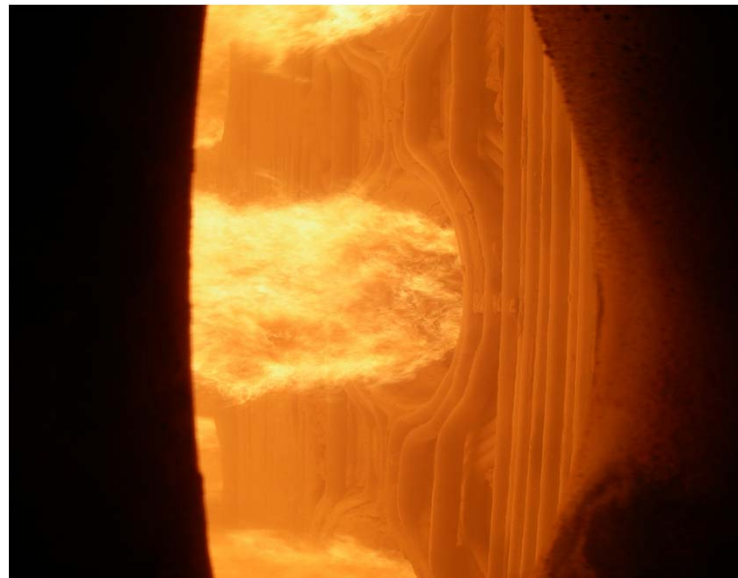


Conclusion

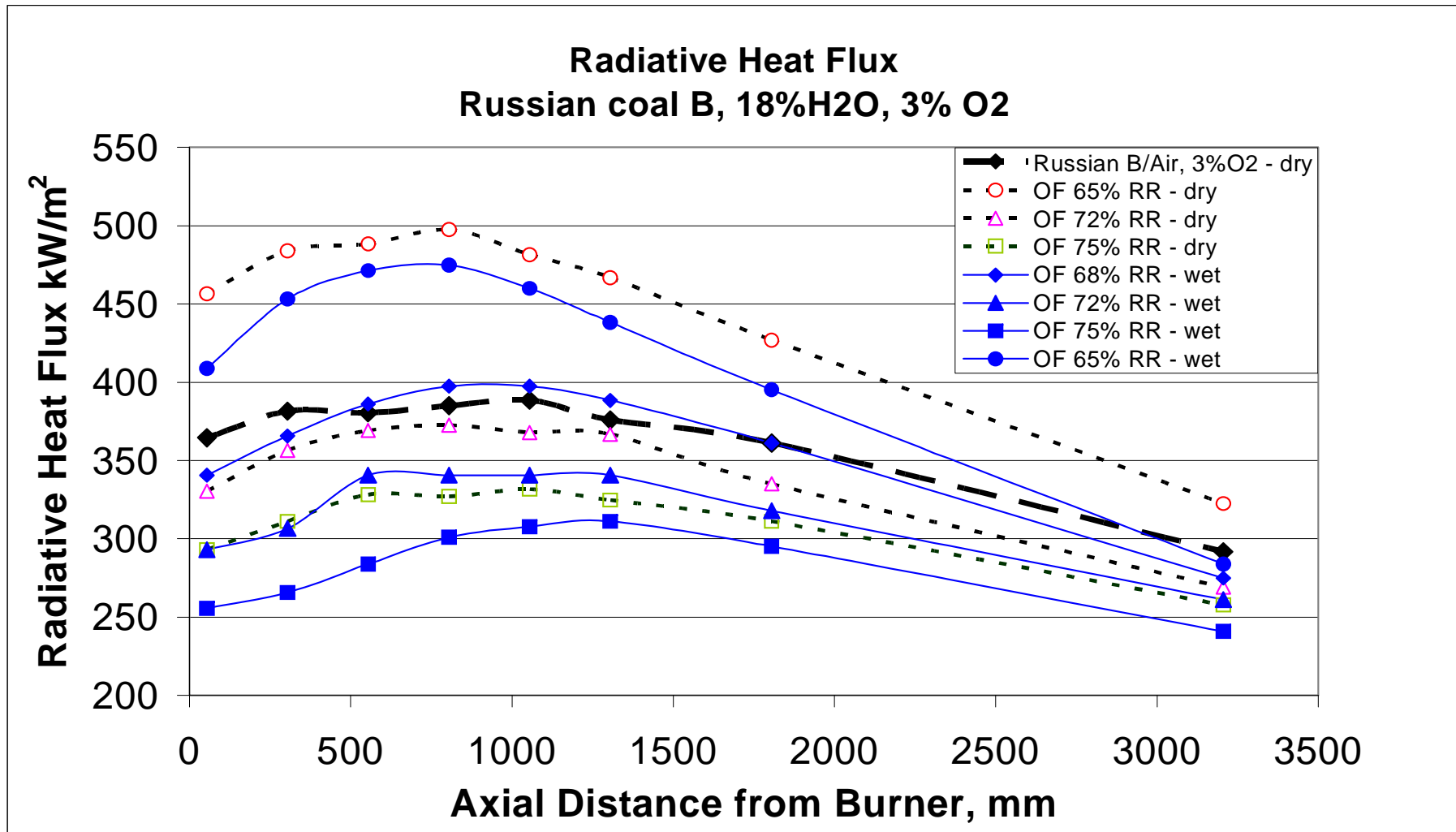
(Biased and do not represent RWE's views!!)

- > Oxyfuel is a better option than post combustion capture
 - Suitable for retrofit
 - Flexibility on fuel
 - It is more flexible than Post Combustion Capture
 - Where the oxygen is injected
 - Recycle rate
 - OFA port options.

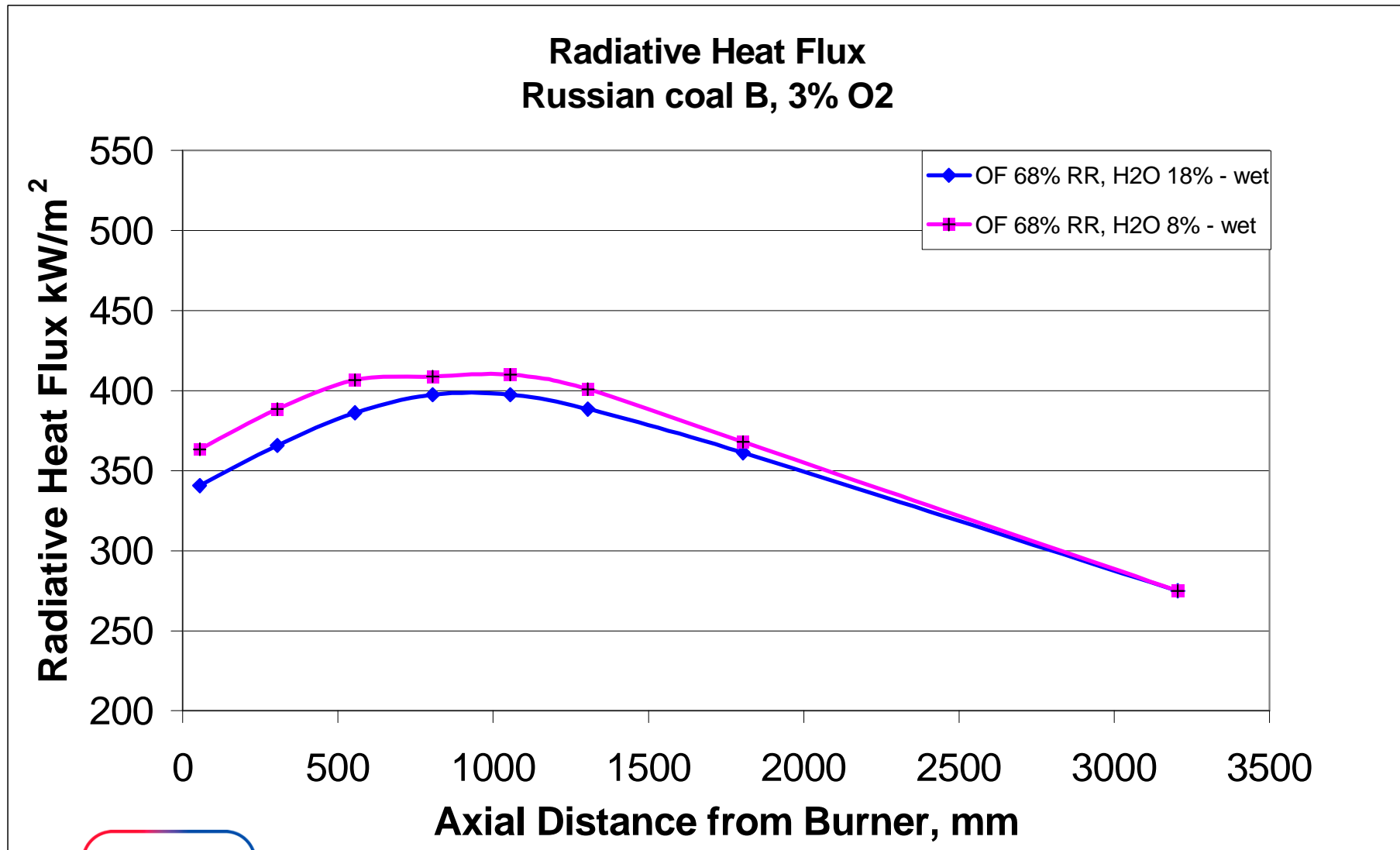
Thank you for your attention.



Latest results – Wet / Dry comparison



Latest results – Wet (8%) / Wet (18%) comparison



Wet (18%) and Dry Recycle Normalised Peak Radiative and Convective Heat Flux

